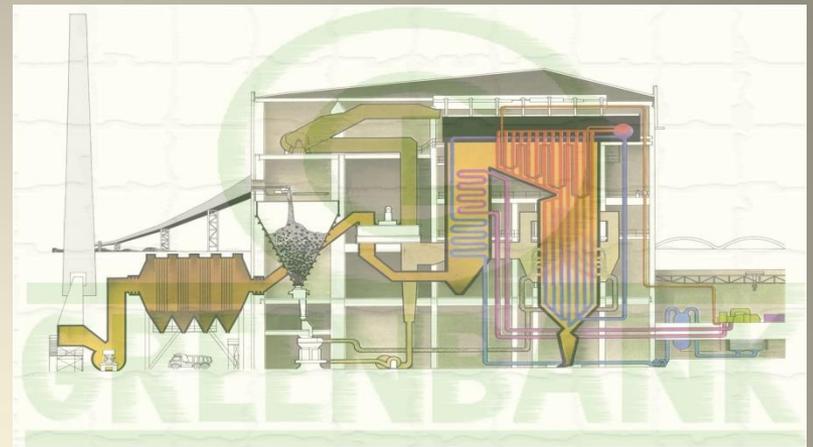




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HEP DYNAMIC CLASSIFIER



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Classification – Impact on Combustion

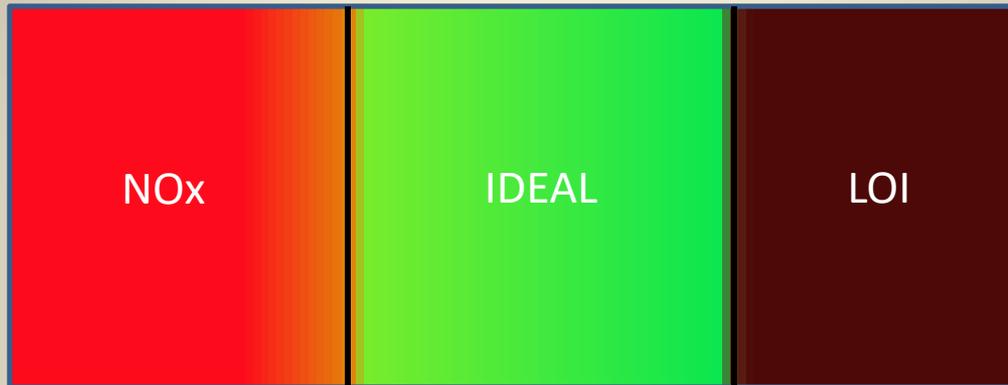
Pulverized Coal Particle Size

1. The particle size distribution of the PF will affect the combustion taking place in the boiler
2. The larger a particle, the lower its surface area: volume ratio
3. Low NO_x coal burners designed for 200 mesh (75 micron) particle size
4. The further from the 200 mesh ideal particle size the worse the impact on the combustion
5. The surface area to volume ratio affects how the particle will combust – primarily, how it will burn
6. Particles that are too large/coarse have an insufficient surface area to combust fully, as well as being physically excessively heavy, and will drop into the ash at the bottom of the furnace
7. Particles that are too small/fine have an excessive surface area and will combust too rapidly, increasing the flame temperature and catalyzing the formation of increased levels of NO_x



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Classification – Impact on Combustion



45 μ m
325 mesh

75 μ m
200 mesh

220 μ m
65 mesh

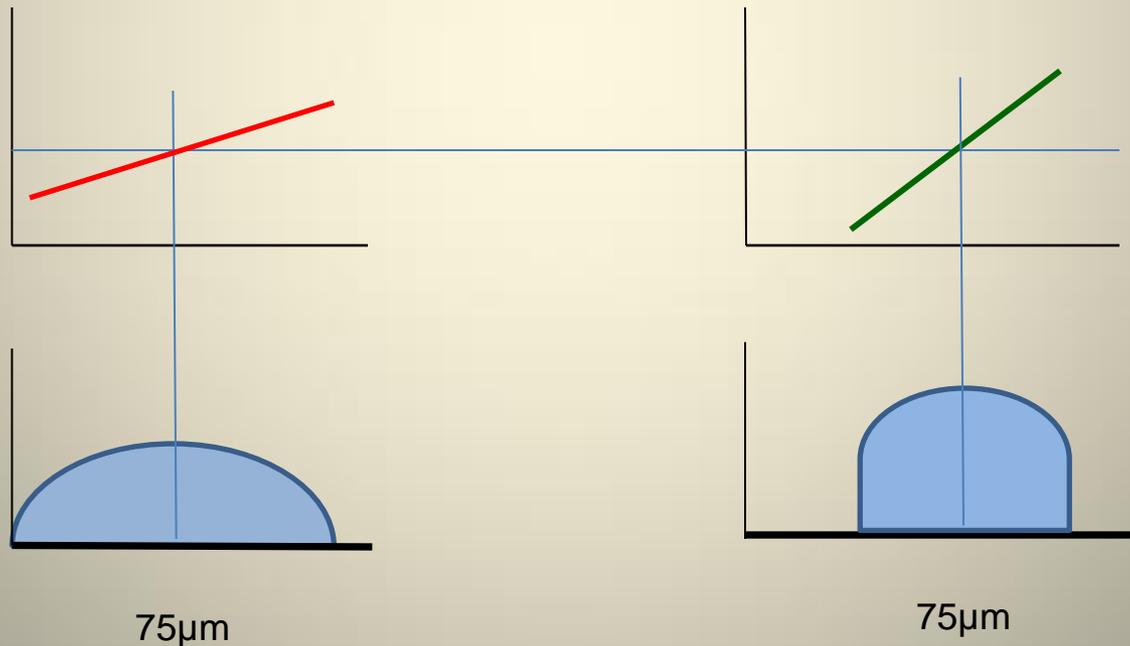


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Classification – Impact on Combustion

Pulverised Coal Particle Size Distribution Variance

1. The slope of the graph is broadly analogous to the variance of the distribution
2. The Rosin Rammler slope gets steeper as the distribution of particle size gets narrower
3. Thus the goal of any classifier design is to minimize/eliminate all particles greater than 65 mesh and less than 325 mesh without increasing mill pressure drop





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Classifier Types

Traditional Static

Base Capacity @ slope 45°

High Performance Static

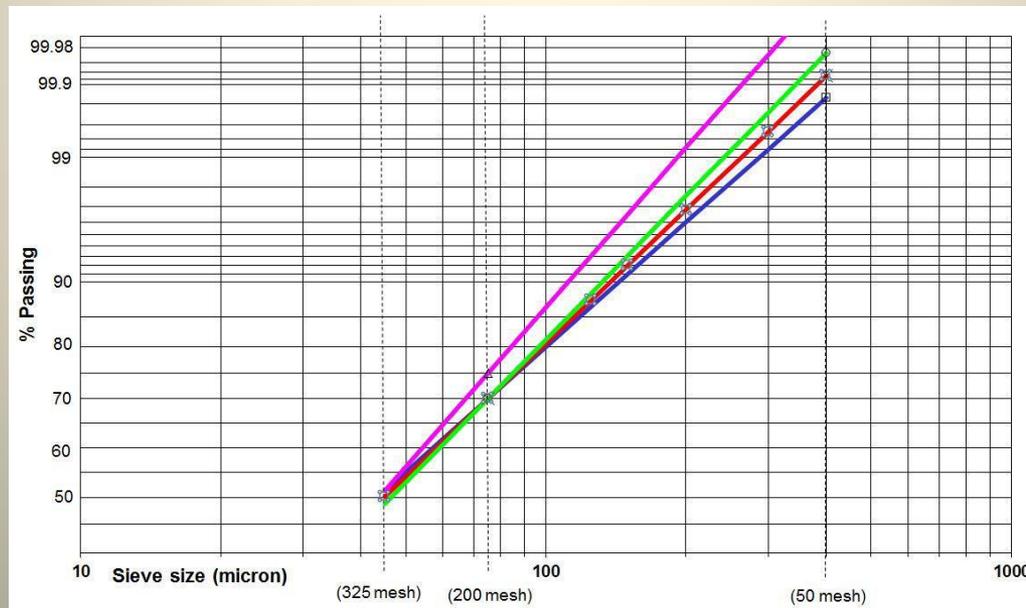
2.5% Capacity = 1.25% on 75 micron @ slope 47°

1st / 2nd Generation Dynamic

5.0% Capacity = 2.50% on 75 micron @ slope 49°

4th Generation Dynamic

15.0% Capacity = 7.50% on 75 micron @ slope 52°





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Brief History of the HEP

The Fuller Co. was founded based on the development of the Kinyon Pump in 1919. The pump provided a safer way to transport pulverized coal to a boiler in a dilute phase pneumatic system and Fuller Co. became a leader in the development of transport and material classification for the coal and cement industry.

In 1983 Fuller began supplying O-Sepa Dynamic Classifiers for coal and cement.

In 1990 the Fuller Co was purchased by FL Smidth of Denmark and had already begun development and sales of the HEP Dynamic Classifier for coal mills with over 350 units installed worldwide

In 1992 Steel and Alloy Utility Products began manufacturing the HEP for Fuller / FLSmidth HEP Dynamic Classifiers sold in the US

In 2016 Greenbank Energy and S&A have begun a joint venture to continue the manufacturing and sales of the product line.



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HEP Classifier Operating Principle

As rotor speed increases,
 F_c increases

As particle size increases,
 F_a decreases

When:

$$F_c - F_a \geq 0$$

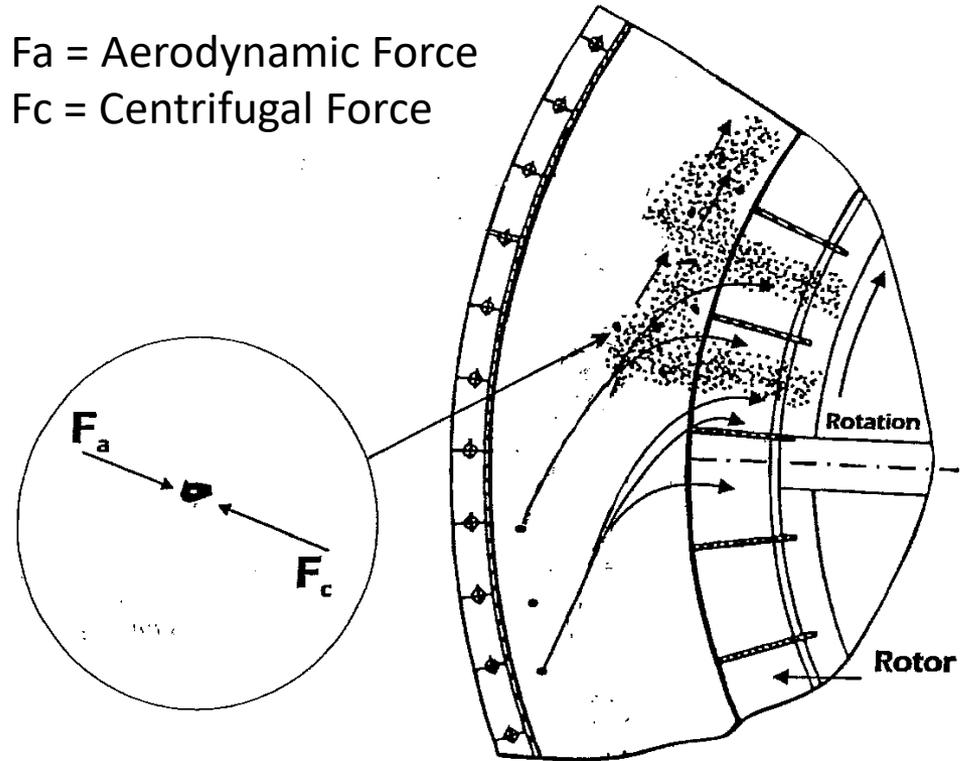
Particle is rejected

$$F_c - F_a < 0$$

Particle is passed through

F_a = Aerodynamic Force

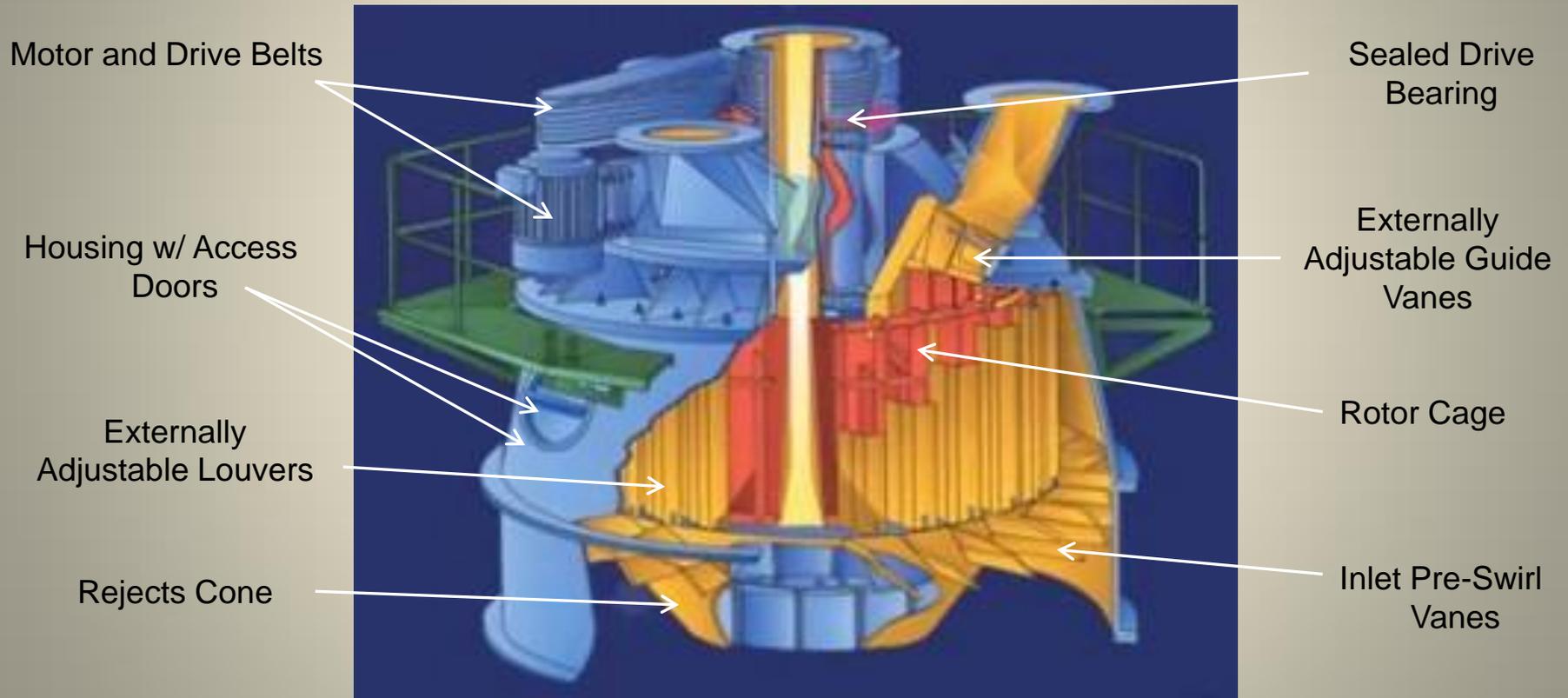
F_c = Centrifugal Force





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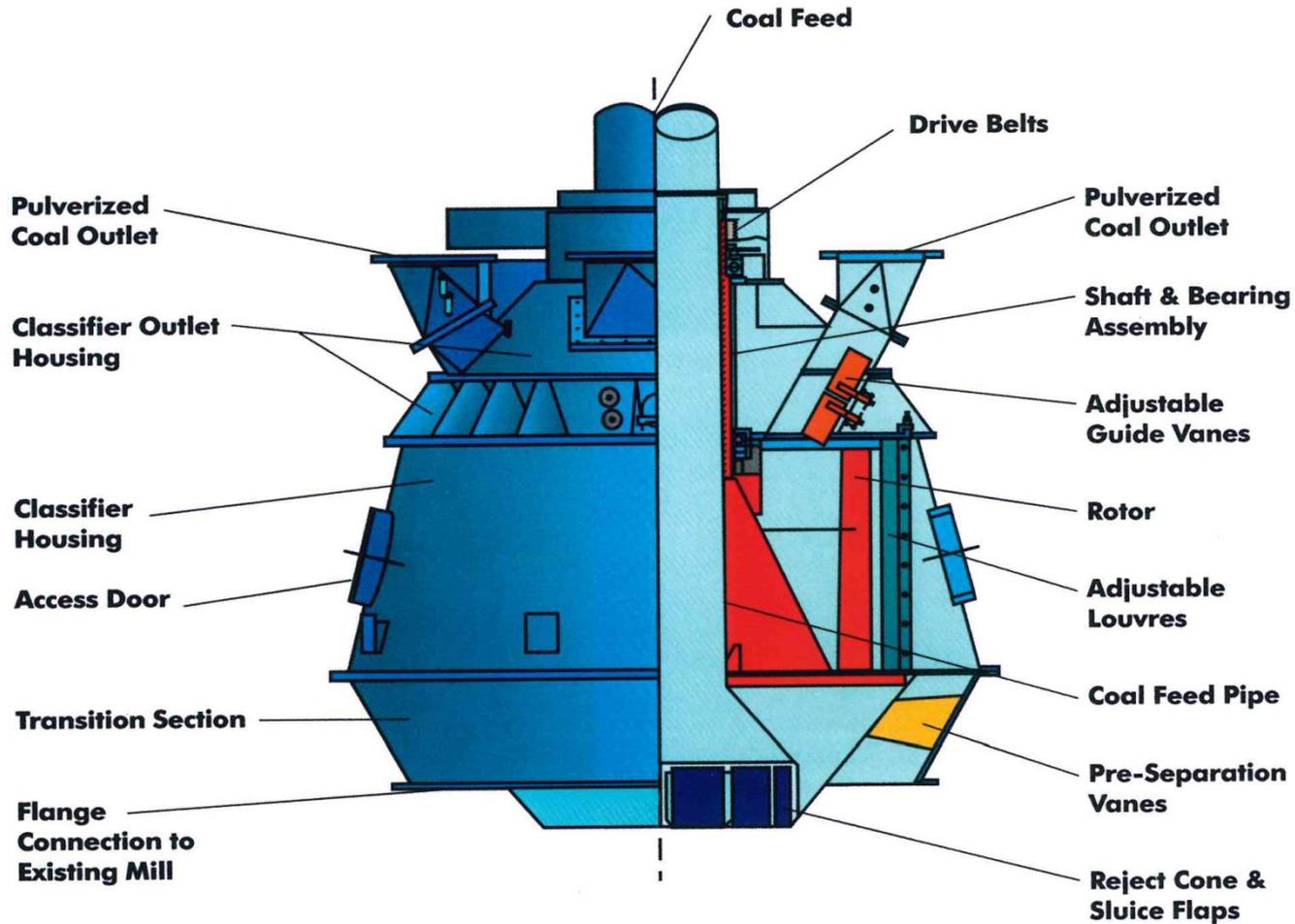
HEP Classifier Design Features





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HEP Classifier Design Features





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HEP Classifier Design Features

Designed specifically for each pulverizer and burner configuration

Wear resistant materials used for extended wear life

Sealed bearing and belt drive system

Side mount rotor drive motor for low profile

Externally adjustable louvers and guide vanes for online balancing

Air/Fuel Ratio adjustable for pipe-to- pipe balance and improved combustion



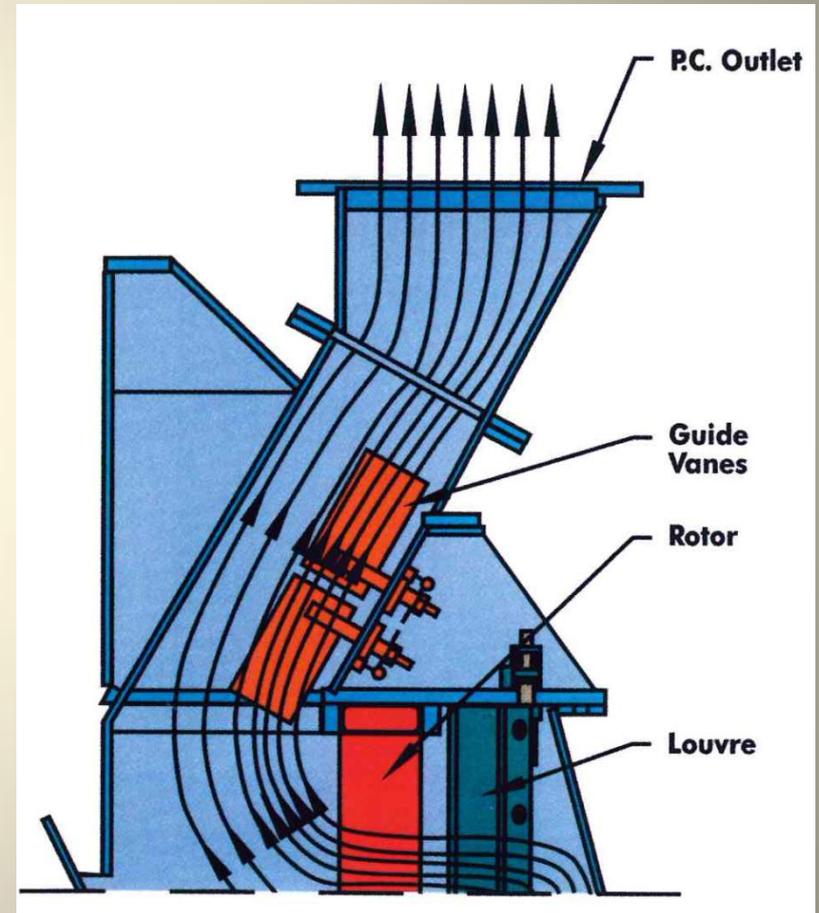
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Improved Air/Fuel Distribution

To maximize the efficiency of low NO_x burners, balanced air/fuel ratios must be delivered burner to burner

Externally adjustable Guide Vanes at the coal pipe outlet can be set to maintain a 7% or better pipe to pipe balance of PF flow.

This insures proper burner function as well as secondary and overfire air utilization to aid in NO_x reduction





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Questions?